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3	ENERGY GAINS OF EUCALYPTUS BY TORREFACTION PROCESS
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14	ABSTRACT
15	The aim of this study was to evaluate the changes in the characteristics of Eucalyptus spp.
16	from Paraíba Valley region, Sao Paulo - Brazil after torrification process. Torrification is
17	a thermochemical process that occurs at temperatures lower than the pyrolysis process as
18	a pretreatment to improve biomass characteristics for use as biofuel energy in power
19	generation. An experimental study was carried out in a batch reactor at three temperatures
20	(240 °C, 260 °C and 280 °C) with residence time of 30 and 60 minutes. At the indicated
21	operating conditions by elemental analysis, higher heating value and thermogravimetric
22	analysis were evaluated. Result showed that there was a reduction in the oxygen/carbon
23	(O/C) and hydrogen/carbon (H/C) ratios, causing an increase in the thermal energy quality

- (O/C) and hydrogen/carbon (H/C) ratios, causing an increase in the thermal energy quality
 of torrified wood, about of 28 % and 47 % at temperatures of 260 °C with residence time
 of 60 minutes and 280 °C with 30 minutes, respectively. A thermogravimetric analysis
 showed that at 260 °C the hemicellulose was almost completely degraded leaving the fuel
 in better conditions for combustion or gasification processes.
- 28 Keywords: Biomass, *Eucalyptus spp.*, pretreatment, thermal characterization,
 29 torrefaction.

INTRODUCTION

The use of biomass for power generation has attracted the attention of several countries 38 and researchers. This is because biomass is a renewable resource and can be used in some 39 processes to replace fossil resources (Sami et al. 2001). In Brazil, biomass has been used 40 for energy generation through the combustion process, being sugarcane bagasse, firewood 41 42 and charcoal widely used. However, wood has a higher preference over because it contains more energy, has a higher yield per area and is considered a neutral biomass, 43 44 that is it has a closed cycle in CO₂ generation (Van der Stelt *et al.* 2011; Arias *et al.* 2008), reducing environmental pollution and the greenhouse effect. 45

Brazil had an area of planted trees of 7,84 million hectares in 2016, with 5,67 million 46 hectares of eucalyptus planted area, 1,58 million hectares with pine and 0,59 of other 47 species. Of the total eucalyptus plantation 41 % is located mainly in the southeastern 48 region, 17 % in the state of São Paulo, second largest eucalyptus producer in the country 49 behind only the state of Minas Gerais. In the last five years the eucalyptus plantation area 50 has been growing around 2,4 % per year, while the pine plantation has been falling at a 51 rate of 0,7 % per year. Of the total eucalyptus planted area, 14 % goes to the steel industry 52 53 as charcoal (IBÁ 2017). A strong advance in the forest area aimed to produce short rotation forests (2 to 3 years), at the same cost as a traditional forest and double the yield, 54 55 reaching up to 55 TBS ha⁻¹ (TBS - ton of dry biomass per hectare), referred to as energy forests (Eufrade et al. 2016; Couto and Dube 2001). Eucalyptus spp. is a promising 56 57 biomass due to its good adaptation in different climatic variations and different species can be used. Ramos-Carmona et al. 2017, comments in his work on the use of fast-58 growing wood species in Colombia, such as *Pinus patula*, for use in power generation 59 through the torrefaction process. 60

However, the use of biomass such as wood has some difficulties considering its direct use as fuel, such as low energy density, which is attributed to the high moisture content, high oxygen/carbon (O/C) ratio leading to low thermal efficiency compromising the calorific power. Biomass also has a fibrous characteristic, making the grinding process difficult, it is hydrophilic causing an increase in transportation costs, handling and storage difficulties, compromising its use in industrial and residential applications through the combustion and gasification process (Saidur *et al.* 2011).

36 37 One way of improving the properties of biomass is to convert it into biofuel through a pretreatment. That can reduce the inconvenience of raw biomass. Torrefaction is a thermal process that occurs between 200 °C to 300 °C, operating with low heating rates under inert atmosphere. During the torrefaction of biomass three products are generated: a) the non-condensable gases, mainly CO_2 and CO; b) the condensed liquid, which is mostly composed of water moisture and acetic acid; and c) the solid product - torrefied biomass - in a dark brown color (Bergman *et al.* 2004).

75 Torrefaction causes changes in the physicochemical properties of biomass. At the 76 beginning of the heating process biomass loses unbound water and as the temperature rises above 160 °C it loses bound water through chemical reactions forming CO₂. During 77 78 heating at 180 °C to 270 °C hemicellulose decomposes and water, CO₂, acetic acid and phenols are lost leading to a darker, more toast-colored biomass (Bergman et al. 2004). 79 80 The volatile compounds have a low calorific value resulting in an increase of the energy density of torrefied biomass. Arias et al. (2008) reported in their work a significant 81 82 improvement and reduction of energy consumption in the milling step of the torrefied wood; this is due to the reduction of the fibrous structure and the lower moisture content 83 prolonging the wood durability during storage (Van der Stelt et al. 2011; Couto and Dube 84 85 2001; Saidur et al. 2011).

There are several studies reporting the effect of the main parameters of the torrefaction 86 process on biomass but we could not identify reports on the characteristics of the 87 *Eucalyptus* in the Paraíba Valley region in the main databases searched. There are many 88 studies by a group of researchers evaluating the characteristics of the Eucalyptus in the 89 state of Minas Gerais (Fialho, et al. 2019; Figueiro, et al. 2019; Pereira et al. 2013), but 90 91 due to the climatic differences, soil type and form in the planting (Santana et al. 2008) it 92 is important to know the behavior of biomass after torrefaction in the region that also has a significant Eucalyptus production. Therefore, the main objective of this work was to 93 evaluate the characteristics of the of Eucalyptus spp. after the torrefaction process. Wood 94 95 from the Paraíba Valley region, located in São Paulo State - Brazil, was studied because the State contributes to the production of *Eucalyptus* wood and seeks other applications 96 97 for wood produced in the region besides production of paper and cellulose, furniture 98 industry and firewood for industry. The samples were wood in their raw form (untreated) and treated/torrefied at temperatures of 240 °C, 260 °C and 280 °C for 30 and 60 minutes. 99 The characterization was performed by elemental analysis, measurement of higher 100

heating value and thermogravimetric analysis, the latter being only in the intermediate
temperature range of 260 °C.

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MATERIAL AND METHODS

104 The raw wood (w) used for torrefaction was *Eucalyptus spp.*, in the form of chips with approximately 10 x 20 mm² after industrial chopper, with 15 % moisture content; the raw 105 wood was dried at 100 °C \pm 5 °C for 24 hours aiming at a uniform moisture content of 106 107 the samples. 300 g samples were used for each torrefaction reaction at temperatures of 240 °C, 260 °C and 280 °C with residence time of 30 and 60 minutes (Romão, et al. 108 109 2016), in a batch reactor at Lorena School of Engineering laboratory, São Paulo, Brazil. The heating of the reactor starts at room temperature (25 °C) with a heating rate of 110 approximately 5 °C·min⁻¹ under nitrogen atmosphere. After reaching the temperature 111 112 selected in the present study, the residence time starts which in the tests were 30 and 60 minutes. After the end of the reaction, the temperature is reduced for cooling and the 113 torrefied sample is removed. Each treatment was carried out in duplicate. 114

115 Mass Yield

The mass yield was obtained according to Bridgeman (2008), dividing the final mass
(torrefied wood - WT) by the initial mass (raw wood - W) for each torrefaction reaction
and multiplying by 100 (in dry basis).

119 Elemental analysis and higher heating value

Elemental analysis was performed using a Perkin Elmer CHNS/O elemental analyzer (in dry basis), the oxygen being calculated by difference. Calorific value was determined in an IKA C2000 basic calorimeter pump according to ASTM D5865 (ASTM 2019); the amount of heat released by combustion represented by mega joule per kilo of solids in dry basis (MJ·kg⁻¹).

125 Thermogravimetric analysis

126 Thermogravimetric analysis (TGA) and its derivative (DTG) were performed in a Perkin 127 Elmer STA 6000 equipment under nitrogen gas atmosphere at a constant flow rate of 128 20 mL·min⁻¹. The samples were ground and sieved and samples of 2,4 mg were selected 129 between sieves of 40 and 60 mesh for analysis. The heating started at 35 °C up to 800 °C 130 at a rate of 10° C·min⁻¹ to evaluate the thermal decomposition profile of raw (W) and torrified wood (WT). For this study samples treated at 260 °C with residence times of 30
and 60 minutes (WT260-30 and WT260-60) were used because this temperature is
typically for torrefaction processes (Romão *et al.* 2016; da Silva *et al.* 2017; ArteagaPérez *et al.* 2015).

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RESULTS AND DISCUSSION

During the torrefaction process changes occur in the main components of biomass due to 136 the increase in temperature, initially affecting hemicellulose and, subsequently, cellulose 137 138 and lignin. Table 1 shows the results obtained for mass yield, elemental analysis and higher heating value of raw and torrified wood at temperatures of 240 °C, 260 °C and 280 139 °C with residence time of 30 min and 60 min. As expected, mass yield decreased from 140 88,5 % to 62,8 % as the temperature and time increased. The results showed that the 141 142 temperature variation had a greater impact on the mass yield than the reaction time. Arias et al. (2008) also reported in their work, with eucalyptus samples treated at the same 143 144 temperature and residence time of 30 minutes, a reduction in mass yield, in the range of 145 82 % to 61%. Even increasing the residence time up to 2 hours there was no significant change in mass yield, mainly between 240 °C and 260 °C. At the first 30 minutes is 146 associated with the decomposition of more reactive components of hemicellulose. As the 147 148 residence time increases, the carbon content increases, and the mass loss occurs due to the decomposition of the less reactive components of hemicellulose. This behavior was 149 150 also observed by Cardona et al. (2019) and Artega-Pérez et al. (2015).

Table 1: Mass yield, elemental analysis and higher heating value of raw wood and

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torrefied wood in different temperatures and residence times.

Item	Wood	WT	WT	WT	WT	WT	WT
	(W)	(240-30)	(240-60)	(260-30)	(260-60)	(280-30)	(280-60)
Mass yield (%)	-	88,46	83,33	83,33	69,67	70,00	62,80
C (%)	45,52	51,10	49,42	52,24	57,14	53,95	58,11
H (%)	6,26	5,57	5,67	5,73	5,32	5,65	5,31
O (%)	46,13	41,61	43,57	35,97	36,47	37,05	25,78
N (%)	0,79	0,00	0,33	4,23	0,00	1,75	9,64
Ratio O/C	0,76	0,61	0,66	0,52	0,48	0,52	0,33
Ratio H/C	1,65	1,31	1,38	1,32	1,12	1,26	1,10
HHV ($MJ \cdot kg^{-1}$)	17,42	20,54	19,35	20,84	22,40	25,61	23,08

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The elemental analysis shows that the carbon content increases with the temperature and residence time while hydrogen and oxygen are reduced. The hydrogen content had a small reduction, while the oxygen of the wood treated at 280 °C for 60 minutes had a 44%

reduction compared to the untreated wood. After the torrefaction process, part of the 157 158 hydrogen and oxygen are removed from the biomass as water and light volatiles, while relatively more carbon is retained. As a consequence, the O/C and H/C ratios were 159 160 reduced to 0,61-0,33 and 1,10-1,31 respectively. Those reductions in the treated fuel will 161 generate less smoke and water vapor during the combustion or gasification process 162 (Saidur *et al.* 2011), increasing the higher heating value of the fuel and giving the hydrophobic characteristic to the treated wood. The calorific value is an important data 163 164 for fuels energy applications. According to Table 1, the calorific value showed an increase 165 of 28 % and 47% in treatments at 260 °C for 60 minutes and 280 °C for 30 minutes, respectively, in relation to raw wood. The value obtained at 260 °C for 60 minutes was 166 similar to that obtained by Arias et al. (2008) (22,8 MJ·kg⁻¹) using eucalyptus, but the 167 value at 280 °C for 30 minutes was higher than that of Arias et al. (2008) (23,4 MJ·kg⁻¹). 168 169 In the present work the torrefaction carried out at 280 °C for 30 minutes showed the highest calorific value with a mass yield of 70%, evidencing the effect of the temperature 170 171 increase and short reaction time as also reported by Chen et al. (2015). At higher temperatures (300 °C) the cellulose also degrades that leads to an increase of the lignin 172 173 (Da Silva et al. 2017); from this temperature onwards the pyrolysis process begins.

174 Thermogravimetric analysis

Thermogravimetric analysis (TGA) evaluates the stability to thermal degradation of the sample and the degradation rate as a function of temperature and time that lead to percentage of sample mass loss; DTG curves refer to the first derivative of the TGA curves and present the mass variation as a function of time, but recorded as a function of temperature. From these analyses it is possible to evaluate the behavior of the main components of biomass (hemicellulose, cellulose and lignin) that have different thermal behaviors, thus making possible to understand the torrefaction process.

Figure 1 presents the curves obtained by TGA and DTG of the raw and torrefied wood 182 samples at 260 °C for 30 and 60 minutes. As can be seen, as the temperature of the 183 184 torrefaction process increases a mass reduction of the samples occurs. The curve indicated 185 by (1) in Figure 1 (1) presents three ranges of thermal degradation: the first between 186 100 °C and 200 °C corresponding to section (a); the interval between (a) and (b) is attributed to wood drying - moisture loss. The other two bands (b) and (c) refer to the 187 degradation of hemicellulose and cellulose, respectively. The second temperature range 188 between 200 °C and 300 °C (b) corresponds mainly to the thermal degradation of 189

hemicellulose, the most reactive polymer, as discussed by several authors (Shen *et al.* 2010; Da Silva *et al.* 2017; Lu *et al.* 2013). The third temperature range (c) between 315
°C and 400 °C corresponds to the degradation of cellulose and the lignin, a macromolecule composed of aromatic chains that is more resistant to thermal degradation
when compared to hemicellulose and cellulose, and its weight loss varies from 150 °C to 900 °C (Yang *et al.* 2007).





Figure 1: TGA / DTG curves of raw and torrefied wood at 260 °C for 30 min and 60 min. 197 The two degradation bands (a) and (b) present in the raw wood related to the presence of 198 moisture and the hemicellulose fraction, respectively, are not present in the torrefied 199 200 wood samples - Figure 1(2) and (3). The absence of the hemicellulose characteristic curve in the shoulder shape in torrefied wood indicates that hemicellulose was almost totally 201 degraded during the heat treatment at 260 °C because it is more reactive due to its 202 amorphous structure (Tumuluru et al. 2010). The cellulose peak is still present due to its 203 204 crystalline structure, more resistant to heat than hemicellulose (Yang et al. 2007). Figure 1(3) shows a small shoulder in the curve near the temperature of 400 °C, 205

suggesting a structural rearrangement in order to obtain a chemically reduced structure of
the lignin, due to the fact that it is in an inert atmosphere at a high temperature. This
modification does not lead to a significant reduction in lignin mass, as can be seen in the
work by Da Silva *et al.* (2016).

CONCLUSIONS

According to the results it was verified that the *Eucalyptus spp*. wood from Paraíba Valley region of São Paulo State - Brazil had its characteristics improved by the torrefaction process aiming to its use as biofuel. Hydrogen and oxygen content reduction led to an increase of the HHV value up to 47 % higher than raw wood. Thermogravimetric analysis of torrified wood WT at 260 °C showed degradation of large part of the hemicellulose which favors an increase in the carbon content and the HHV value.

The torrefaction is a beneficial pretreatment for Eucalyptus *spp*. wood. It promotes changes in its chemical composition leading to an attractive renewable fuel for energy

220 generation thus contributing to the reduction of greenhouse effect gases.

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REFERENCES

American Society for Testing and Materials. 2019. ASTM D5865-19: Standard Test
 Method for Gross Calorific Value of Coal and Coke. ASTM International. West
 Conshohocken, PA, USA. <u>https://doi.org/10.1520/D5865_D5865M-19.</u>

Arias, B.R.; Pevida, C.G.; Fermoso, J.D.; Plaza, M.G.; Rubiera, F.G.; Pis Martinez,
 J.J. 2008. Influence of torrefaction on the grindability and reactivity of woody biomass.
 Fuel Process Technol 89(2): 169–175. https://dx.doi.org/10.1016/j.fuproc.2007.09.002.

Artega-Pérez, L.E.; Segura, C.; Bustamante-García, V.; Cápiro, O.G.; Jiménez, R.
2015. Torrefaction of wood and bark from *Eucalyptus globulus* and *Eucalyptus nitens*:
Focus on volatile evolution vs feasible temperatures. *Energy* 93: 1731-1741.
https://doi.org/10.1016/j.energy.2015.10.007.

Bergman, P.C.A.; Boersma, A.R.; Kiel, J.H.A.; Prins, M.J.; Ptasinski, K.J.; Janssen,
F.J.J.G. 2004. *Torrefaction for entrained-flow gasification of biomass*. (ECN-C; Vol.
2005067). Petten: Energieonderzoek Centrum Nederland. Netherlands.
https://pure.tue.nl/ws/portalfiles/portal/3167898/638046.pdf.

Bridgeman, T.G.; Jones, J.M. 2008. Torrefaction of reed canary grass, wheat straw and
willow to enhance solid fuel qualities and combustion properties. *Fuel* 87(6): 844-856.
https://doi.org/10.1016/j.fuel.2007.05.041.

Cardona, S.; Gallego, L.J.; Valencia, V.; Martinez, E.; Rios, L.A. 2019. Torrefaction
of *Eucalyptus*-tree residues: A new method for energy and mass balances of the process
with the best torrefaction conditions. *Sustainable Energy Technologies and Assessments*31: 17-24. <u>https://doi-org.ez67.periodicos.capes.gov.br/10.1016/j.seta.2018.11.002.</u>

Chen, W.H.; Huang, M.Y.; Chang, J.S.; Chen, C.Y.; Lee, W.J. 2015. An energy
analysis of torrefaction for upgrading microalga residue as a solid fuel. *Bioresour Technol*185: 285-293. https://doi.org/10.1016/j.biortech.2015.02.095.

Couto, L.; Dube, F. 2001. The status and practice of forestry in Brazil at the beginning
of the 21st century: A review. *Forest Chron* 77(5): 817-830.
https://doi.org/10.5558/tfc77817-5.

Da Silva, C.M.S.; Vital, B.R.; Carneiro, A.C.O.; Costa, E.V.S.; Magalhaes, M.A.; 254 Trugilho, P.F. 2017. Structural and compositional changes in eucalyptus wood chips 255 subjected dry torrefaction. Prod 109: 598-602. 256 to Ind Crop http://dx.doi.org/10.1016/j.indcrop.2017.09.010. 257

Da Silva, C.M.S.; Carneiro, A.C.O.; Pereira, B.L.C.; Vital, B.R.; Alves, I.C.N.;
Magalhães, M.A. 2016. Stability to thermal degradation and chemical composition of
woody biomass subjected to the torrefaction process. *Eur J Wood Wood Prod* 74(6): 845850. <u>https://doi.org/10.1007/s00107-016-1060-z.</u>

Eufrade, H.J.; Melo, R.X.; Sartori, M.M.P.; Guerra, S.P.S.; Ballarin, A.W. 2016.
Sustainable use of eucalypt biomass grown on short rotation coppice for bioenergy. *Biomass Bioenerg* 90: 15-21. http://dx.doi.org/10.1016/j.biombioe.2016.03.037.

Fialho, L.F.; Carneiro, A.C.O.; Carvalho, A.M.M.L.; Figueiró, C.G.; Da Silva,
C.M.S.; Magalhães, M.A.; Peres, L.C. 2019. Bio-coal production with agroforestry
biomasses in Brazil. *Maderas-Cienc Tecnol* 21(3): 357-366.
http://dx.doi.org/10.4067/S0718-221X2019005000308.

269 Figueiró, C.G.; Vital, B.R.; Carneiro A.C.O.; Silva, C.M.S.; Magalhães, M.A.;

Fialho, L.F.; 2019. Energy valorization of woody biomass by torrefaction treatment: A

271 Brazilian experimental study. *Maderas-Cienc Tecnol* 21(3): 297-304.
 272 https://doi.org/10.4067/S0718-221X2019005000302.

Indústria Brasileira De Árvores. IBA. 2017. *Relatório 2017*. IBÁ. Brazil. 80p.
 https://iba.org/images/shared/Biblioteca/IBA_RelatorioAnual2017.pdf.

Lu, K.M.; Lee, W.J.; Chen, W.H.; Lin, T.C. 2013. Thermogravimetric analysis and
kinetics of co-pyrolysis of raw/torrefied wood and coal blends. *Appl Energ* 105: 57-65.
http://dx.doi.org/10.1016/j.apenergy.2012.12.050.

278 Pereira, B.L.C; Carneiro, A.C.O.; Carvalho, A.M.M.L.; Trugilho, P.F.; Melo,

279 I.C.N.A.; Oliveira, A.C.; 2013. Study of termal degradation of Eucalyptus wood by

- thermogravimetry and calorimetry. *Rev Arvore* 37(3): 567-576.
 <u>http://www.redalyc.org/articulo.oa?id=48828116020.</u>
- Ramos-Carmona, S.; Pérez, J.F.; Pelaez-Samaniego, M.R.; Barrera, R.; Garcia Perez, M. 2017. Effect of torrefaction temperature on properties of Patula pine. *Maderas*-
- 284 *Cienc Tecnol* 19(1): 39 50. http://dx.doi.org/10.4067/S0718-221X2017005000004.
- Romão, E.L.; Dias, I.A., Conte, R.A.; Pinatti, D.G. 2016. Avaliação do efeito da
 torrefação de biomassa lenhosa visando à produção de biocombustível para fins
 energéticos. In *XXI Congresso Brasileiro de Engenharia Química COBEQ*, Fortaleza,
 CE, Brazil. (in portuguese).
 https://proceedings.science/proceedings/44/ papers/40957/download/fulltext file1.
- Saidur, R.; Abdelaziz, E.A.; Demirbas, A.; Hossain, M.S.; Mekhilef, S. 2011. A
 review on biomass as a fuel for boilers. *Renew Sust Energ Rev* 15(5): 2262–2289.
 https://doi.org/10.1016/j.rser.2011.02.015.
- Sami, M.; Annamalai, K.; Wooldridge, M. 2001. Co-firing of coal and biomass fuel
 blends. *Prog Energ Combust* 27(2): 171–214. <u>https://doi.org/10.1016/S0360-</u>
 1285(00)00020-4.
- Santana, R.C.; Barros, N.F.; Leite, H.G.; Comerford, N.B.; Novais, R.F. 2008.
 Biomass estimation of Brazilian eucalypt plantations. *Rev Arvore* 32(4): 697-706.
 https://doi.org/10.1590/S0100-67622008000400011.
- Tumuluru, J.S.; Sokhansanj, S; Wright, C.T.; Boardman, R.D. 2010. Biomass
 Torrefaction Process Review and Moving Bed Torrefaction System Model Development.
 Idaho National Laboratory Biofuels and Renewable Energy, Technologies Department
 Idaho Falls, EUA. https://inldigitallibrary.inl.gov/sites/sti/4734111.pdf.
- Van der Stelt, M.J.C.; Gerhauser, H.; Kiel, J.H.A.; Ptasinski, K.J. 2011. Biomass
 upgrading by torrefaction for the production of biofuels: A review. *Biomass bioenerg* 35:
 3748-3762. https://doi.org/10.1016/j.biombioe.2011.06.023.
- Yang, H.; Yan, R.; Chen, H.; Lee, D.H.; Zheng, C. 2007. Characteristics of
 hemicellulose, cellulose and lignin pyrolysis. *Fuel* 86: 1781-1788.
 https://doi.org/10.1016/j.fuel.2006.12.013.